

Particle hydrodynamics: from molecular to colloidal fluids

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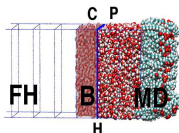
von Neumann Symposia, Snowbird. July 2011

Multiscale approaches for complex liquids

Domain decomposition

type A

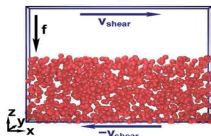
Molecular detail,
interfaces, surfaces,
macromolecule -fluid interaction



shear flows ✓
sound, heat ✓
large molecules ✓
multispecies ✗
electrostatics ✗

Eulerian-Lagrangian Solute-solvent hydrodynamic coupling

Suspensions
of colloids or polymers,
small particles in flow



Point particle approximation:
Stokes drag (point particle),
Faxen terms (**finite size effects**)
Basset **memory effects**...
Force Coupling
particles of finite size
Direct simulation
Immersed boundaries

Patch dynamics HMM Velocity-Stress coupling

type B

Non-Newtonian fluids
Unknown constitutive relation
polymer melts...

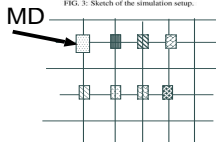


FIG. 3: Sketch of the simulation setup.

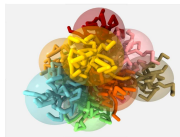
MD nodes used to
evaluate the **local stress**
for the Continuum solver.

Continuum solver provides
the local **velocity gradient**
imposed at each MD node.

how to "lift MD" ✗

Coarse-grained dynamics

How to reduce the
degrees of freedom
and keep the
underlying **dynamics**



diffusion ✓
viscosity ✓
anisotropy ✗
(nematics...)

- Particle hydrodynamics
 - Florencio Balboa (Univ. Autonoma Madrid)
 - Aleks Donev (Courant Institute, New York)
 - Ignacio Pagonabarraga (Univ. Barcelona)
- Open fluctuating hydrodynamics
 - Anne Dejoan (CIEMAT)
- Hybrid molecular-continuum hydrodynamics
 - Gianni De Fabritiis (U. Pompeu Fabra, Barcelona)
 - P. V. Coveney (UCL, London)
 - E. Flekkoy (Oslo Univ.)
 - Jason Reese (U. StrathClyde, Glasgow) (new)
- Adaptive resolution in HybridMD
 - Matej Praprotnik (National Inst. Chem. Ljubljana)
 - Kurt Kremer (Max-Planck, Mainz)
- Coarse-grained dynamics
 - Pep Español (UNED)
 - Eric vanden-Eijnden (Courant Institute, NY)

Outline of the talk

- **Domain decomposition**

- OPENMD: generalized open boundary conditions for MD
- HYBRIDMD: Particle-continuum hybrid
- ADDRESS: Adaptive Resolution *mesoscopic layer*.

- Particle hydrodynamics:
an Eulerian-Lagrangian approach

- DIRECT FORCING theoretical background
- Tests: manipulation of colloidal particles using ultrasound

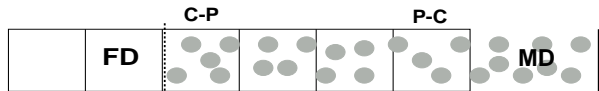
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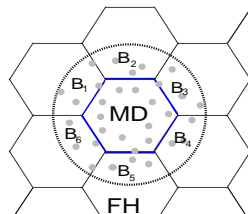
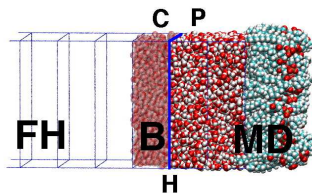
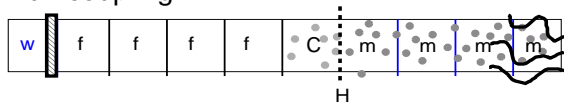
Hybrid particle-continuum schemes

Recent review: R. Delgado-Buscalioni, in "Numerical Analysis and Multiscale Computations", Lect. Notes Comput. Sci. Eng., Volume 82, Springer Verlag (to appear)"

State-coupling



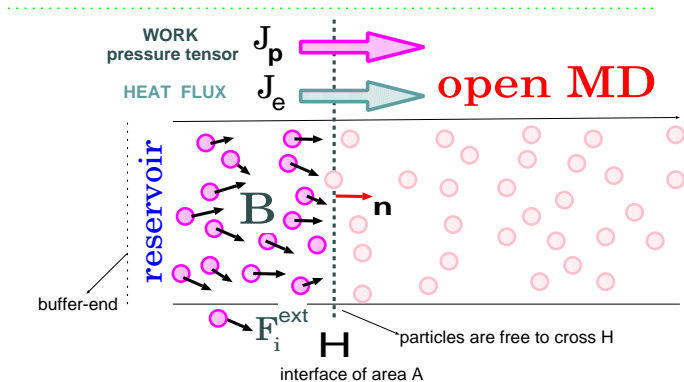
Flux-coupling



Open Molecular Dynamics

Open MD via external forces

$$m\ddot{\mathbf{r}}_i = \mathbf{f}_i(\{\mathbf{r}\}) + \mathbf{f}_i^{\text{ext}}$$



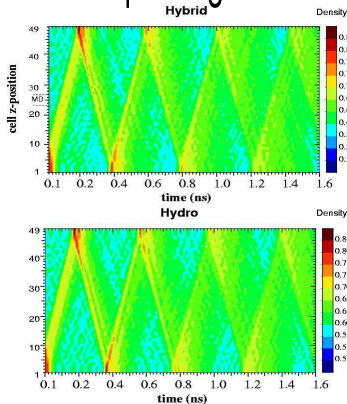
Hybrid MD-FH: Sound

De Fabritiis, R.D-B and P. Coveney, PRL, 97 (2006)

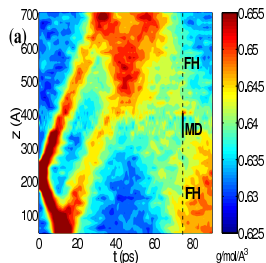
RDB and De Fabritiis PRE 76, 036709 (2007)

Important: Mass conservation and similar sound velocities (EOS) across H

liquid argon



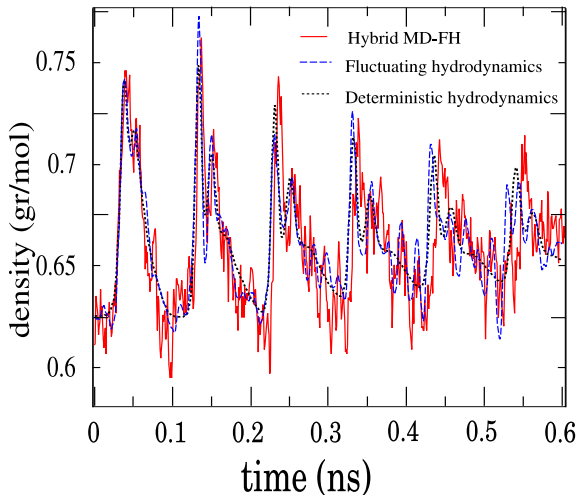
water



Hybrid MD-Fluctuating Hydrodynamics

Some test cases: sound

RDB and De Fabritiis PRE 76, 036709 (2007)

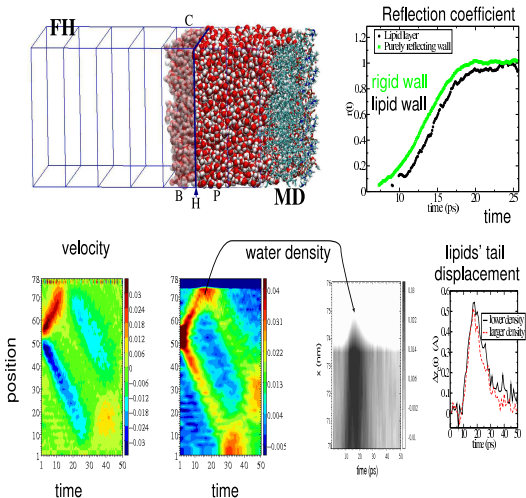


Hybrid MD-Fluctuating Hydrodynamics

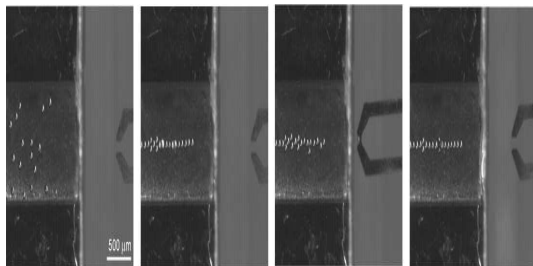
Collision of sound waves against DMPC lipid layer

De Fabritiis, R.D-B and P. Coveney, PRL, 97 (2006)

RDB et al, Proc IMechE, Part C: J Mech. Eng. Sci. **222** (2008)



The Direct Forcing Method for particle hydrodynamics



(a)

(b)

(c)

(d)

Micromanipulation of micron size particles with ultrasound. Jürg Dual group, ETH

Direct Forcing for Point particle hydrodynamics.

Motivation

- **The Immersed Boundary method** $\dot{\mathbf{R}}_p = \mathbf{u}_p$
 - Fluid-structure interaction. $\mathbf{F}_{fp} = \mathbf{F}(\{\mathbf{R}_p\})$
 - No inertial forces
- **The Stokes coupling method** $\ddot{\mathbf{R}}_p = (\xi/M) (\mathbf{u}_p - \mathbf{V}_p)$
 - A practical relaxation method to achieve $\mathbf{u} = \mathbf{v}_p$ [Ladd, Dünweg].
 - Limited to low Reynolds and small velocity gradients [Maxey, Riley]
 - Response time τ limited by the friction time $\tau > M/\xi$
 - Cannot solve ultrasound-matter interaction [Mazur, Bedeaux] or fast inertial forces (turbulence).
- **Direct Forcing method** $M_p \ddot{\mathbf{R}}_p = \mathbf{F}_p(\mathbf{V}_p, \mathbf{u})$
 - The fluid-particle force ensures no-slip at the particle site.
 - Instantaneous momentum transfer: particle inertia, fast forcing (ultrasound, etc).
 - Straightforward implementation from Stokes

Equations of motion

- Particle

$$\dot{\mathbf{R}}_p = \mathbf{V}_p \quad (1)$$

$$M_p \frac{d\mathbf{V}_p}{dt} = - \int_{\mathcal{V}_p} \nabla \cdot \mathcal{P} d\mathbf{r}^3 + \mathbf{F}_{\text{ext}} \quad (2)$$

$$I_p \frac{d\boldsymbol{\Omega}_p}{dt} = - \oint_S (\mathbf{r} - \mathbf{R}_p) \times \mathcal{P} \cdot \mathbf{n} d\mathbf{r}^2 + \mathbf{F}_{\text{ext}} \times \mathbf{r} \quad (3)$$

- Fluid (fluctuating hydrodynamics)

$$\frac{\partial \rho}{\partial t} = -\nabla \cdot \mathbf{g} \quad (4)$$

$$\frac{\partial \mathbf{g}}{\partial t} = -\nabla \cdot \boldsymbol{\Pi} + \mathbf{f}. \quad (5)$$

Stress tensor $\boldsymbol{\Pi} = \mathbf{g}\mathbf{u} + \mathcal{P}$ with $\mathcal{P} = \pi \mathbf{1} + \eta [\nabla \mathbf{u}]^{\text{sym}} + \tilde{\mathcal{P}}$

Boundary conditions

- **Particle surface resolved**

$$\mathbf{u} = \mathbf{V}_p + \Omega \times (\mathbf{r} - \mathbf{R}_p) \quad (6)$$

$$\rho = 0 \forall \mathbf{r} \in \mathcal{V}_p \quad (7)$$

where $\mathbf{r} - \mathbf{R}_p = R \mathbf{n}$

- **Single site approach (pointwise)**

$$\mathbf{u} = \mathbf{V}_p \text{ at } \mathbf{r} = \mathbf{R}_p \quad (8)$$

Momentum balance

- Integrate momentum eq. over the whole domain

$$\frac{d}{dt} \int \mathbf{g} \, d\mathbf{r}^3 = \int \nabla \cdot \mathcal{P} \, d\mathbf{r}^3 + \int \mathbf{f} \, d\mathbf{r}^3 \quad (9)$$

- Fluid-particle interaction is short (microscopic) ranged

$$\int \mathbf{f} \, d\mathbf{r}^3 = \int_{\cup \mathcal{V}_p} \mathbf{f} \, d\mathbf{r}^3 \quad (10)$$

- *Non-overlapping* particle volumes

$$\int_{\cup \mathcal{V}_p} \mathbf{f} \, d\mathbf{r}^3 = \sum_p \int_{\mathcal{V}_p} \mathbf{f} \, d\mathbf{r}^3 = \sum_p \mathbf{F}_p \quad (11)$$

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Momentum balance and particle eq. motion

- Integrating over one particle volume:

$$\frac{d}{dt} \int_{\mathcal{V}_p} \mathbf{g} \, d\mathbf{r}^3 = \int_{\mathcal{V}_p} \nabla \cdot \mathcal{P} \, d\mathbf{r}^3 + \mathbf{F}_p \quad (12)$$

$$\text{recall } M_p \frac{d\mathbf{V}_p}{dt} = - \int_{\mathcal{V}_p} \nabla \cdot \mathcal{P} \, d\mathbf{r}^3 + \mathbf{F}_{\text{ext}} \quad (13)$$

- Particle equation of motion

$$M_p \frac{d\mathbf{V}_p}{dt} = \frac{d}{dt} \int_{\mathcal{V}_p} \mathbf{g} \, d\mathbf{r}^3 - \mathbf{F}_p + \mathbf{F}_{\text{ext}} \quad (14)$$

- Incompressible fluid: $\int_{\mathcal{V}_p} \mathbf{g} \, d\mathbf{r}^3 = \rho \mathcal{V}_p \langle \mathbf{u} \rangle_p = \rho \mathcal{V}_p \mathbf{V}_p$

$$\Delta M_p \frac{d\mathbf{V}_p}{dt} = -\mathbf{F}_p + \mathbf{F}_{\text{ext}} \quad (15)$$

Archimedes Eureka: Particle mass excess $\Delta M_p = M_p - m_p$
with $m_p = \rho \mathcal{V}_p$ (evacuated fluid mass).

Momentum balance and particle eq. motion

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The particle-fluid force

- Impose zero relative velocity at particle site: $\langle \mathbf{u} \rangle_p = \mathbf{V}_p$
- Incompressible case
Integrate momentum $\mathbf{g} = \rho \mathbf{u}$ over particle volume \mathcal{V}_p and time Δt :

$$\rho \langle \mathbf{u} \rangle_p(t + \Delta t) = \rho \tilde{\mathbf{u}}_p + \frac{1}{\mathcal{V}_p} \int_t^{t+\Delta t} \mathbf{F}_p(t') dt'. \quad (16)$$

- **Pointwise approach:** volume averaged quantities:
 $\langle \mathbf{u} \rangle_p \mathcal{V}_p \equiv \int_{\mathcal{V}_p} \mathbf{u} dr^3$
- The *unperturbed* fluid velocity field is

$$\rho \tilde{\mathbf{u}}_p = \rho \langle \mathbf{u} \rangle_p(t) - \int_t^{t+\Delta t} \langle \nabla \cdot \boldsymbol{\pi} \rangle_p(t') dt', \quad (17)$$

- The “stick” constraint $\langle \mathbf{u} \rangle_p = \mathbf{V}_p$ in Eq. (16) yields

$$\int_t^{t+\Delta t} \mathbf{F}_p(t') dt' = \rho \mathcal{V}_p [\mathbf{V}_p(t + \Delta t) - \tilde{\mathbf{u}}_p]. \quad (18)$$

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Eulerian-Lagrangian transformations

- Particles move in continuum (Lagrangian) space $\mathbf{R}_p \in \mathbb{R}$.
- Fluid solved at discrete set of Eulerian nodes \mathbf{r}_i .
- Communication requires two operations:

• Interpolation of the unperturbed fluid velocity at particle sites

- Operators in discrete form: $\delta_{ip} = \delta_h(|\mathbf{r}_i - \mathbf{R}_p|)$

$$\text{Interpolation } \phi_p^I = \sum_i \delta_{ip}^I \phi_i \text{ note : } \langle \phi \rangle_p \rightarrow \phi_p^I \quad (19)$$

$$\text{Spreading } \phi_i^S = \sum_p \delta_{ip}^S \phi_p \quad (20)$$

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 - **Interpolation** of the unperturbed fluid velocity at particle site
 - **Spreading** of the particle-fluid force to Eulerian fluid variables
- Operators in discrete form: $\delta_{ip} = \delta_h(|\mathbf{r}_i - \mathbf{R}_p|)$

$$\text{Interpolation } \phi_p^I = \sum_i \delta_{ip}^I \phi_i \text{ note : } \langle \phi \rangle_p \rightarrow \phi_p^I \quad (19)$$

$$\text{Spreading } \phi_i^S = \sum_p \delta_{ip}^S \phi_p \quad (20)$$

with $\phi_i = \phi(\mathbf{r}_i)$ and $\phi_p = \phi[\mathbf{R}_p]$.

Consistency: spreading + interpolation = identity

- It will soon be clear why we need **adjoint operations**:
 spreading ϕ_p gives $\phi_i^S = \sum_p \phi_p \delta_{ip}^S$ and
 interpolation back $\phi_p^{SI} = \sum_q [\sum_i \delta_{ip}^I \delta_{iq}^S] \phi_q$.

$$\text{Therefore } \phi_p^{SI} = \phi_p \text{ if } \sum_i \delta_{ip}^I \delta_{iq}^S = \delta_{pq}^{\text{kr}} \quad (21)$$

where δ_{pq}^{kr} is the Kronecker delta.

Note that Interpolation+Spreading is **not** the identity

- However IB kernels satisfy a weaker property

$$\sum_i \delta_{ip}^I \delta_{ip}^S = 1 \quad (22)$$

- BUT: P. (21) = (22) + *non-overlapping kernels*.
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Immersed Boundary (IB) Kernels (*Peskin*)

- Constructed with a soft function of compact support:

$$\delta_h(\mathbf{r}) = \phi(x/h)\phi(y/h)\phi(z/h)$$

$$\phi(u) = \begin{cases} \frac{1}{3}(1 + \sqrt{1 - 3u^2}) & 0 \leq |u| \leq \frac{1}{2} \\ \frac{1}{6}(5 - 3|u| - \sqrt{-2 + 6|u| - 3u^2}) & \frac{1}{2} \leq |u| \leq \frac{3}{2} \\ 0 & \frac{3}{2} \leq |u| \end{cases}$$

- Satisfying

$$\sum_i \delta_h(\mathbf{r}_i - \mathbf{R}) = 1 \quad (23)$$

$$\sum_i \delta_h^2(\mathbf{r}_i - \mathbf{R}) = 1/c \quad (24)$$

$$\sum_i (\mathbf{r}_i - \mathbf{R})\delta_h(\mathbf{r}_i - \mathbf{R}) = 0 \quad (25)$$

where $c = 8$ for the three point base kernel ϕ .

Interpolation/Spreading pair properties

- Interpolation and spreading based on the same IB kernel:

$$\delta_{ip}^I \equiv \delta_h(\mathbf{r}_i - \mathbf{R}_p) \quad (26)$$

$$\delta_{ip}^S \equiv c \delta_h(\mathbf{r}_i - \mathbf{R}_p) \quad (27)$$

- **Normalization**

$$\sum_i h^3 \delta_{ip}^I = h^3 \quad (28)$$

$$\sum_i h^3 \delta_{ip}^S = \mathcal{V}_p \quad (29)$$

Particle effective volume: from (29) and (27): $\mathcal{V}_p = c h^3$

For the 3 point kernel $c = 8$

Time integration, some notations

- System evolving in discrete times $t_n = n \Delta t$.
- The time integral is noted as

$$\bar{\phi} \equiv \frac{1}{\Delta t} \int_{t_n}^{t_{n+1}} \phi(t) dt \quad (30)$$

- The interpolator and spreading operators depend on time via the particle position.

$$\delta_{ip}^I \equiv \delta^I(|\mathbf{r}_i - \mathbf{R}_p(t_n)|) \quad (31)$$

- Interpolation at equal times: $\mathbf{u}_p^n = \sum_i \delta_{ip}^I \mathbf{u}_i^n$
- Interpolation at *unequal* times: $\mathbf{u}_{p^{n+1}}^n = \sum_i \delta_{ip^{n+1}}^I \mathbf{u}_i^n$

Time integration: the algorithm

- 1) Unperturbed Eulerian velocity $\rho \tilde{\mathbf{u}}_i = \rho \mathbf{u}_i^n - \overline{[\nabla \cdot \mathbf{\Pi}]_i} \Delta t$
- 2) Particle positions $\mathbf{R}_p^{n+1} = \mathbf{R}_p^n + \overline{\mathbf{V}_p} \Delta t$
- 3) Unperturbed Lagrangian velocity $\tilde{\mathbf{u}}_p = \sum_i \delta_{ip}^I \tilde{\mathbf{u}}_i$
- 4) Particle velocity $\mathbf{V}_p^{n+1} = \frac{\delta M_p}{M_p} \mathbf{V}_p^n + \frac{m_p}{M_p} \tilde{\mathbf{u}}_p + \frac{\overline{\mathbf{F}_{\text{ext}} \Delta t}}{M_p}$
 $M_p \equiv \delta M_p + m_p$
- 5) Force spreading $\overline{\mathbf{f}}_i \Delta t = \rho \sum_p [\mathbf{V}_p^{n+1} - \tilde{\mathbf{u}}_p] \delta_{ip}^S$

Check:

$$\mathbf{u}_p = \tilde{\mathbf{u}}_p + \sum_q (\mathbf{V}_q - \tilde{\mathbf{u}}_q) \sum_i \delta_{ip}^I \delta_{iq}^S = \tilde{\mathbf{u}}_p + \sum_q (\mathbf{V}_q - \tilde{\mathbf{u}}_q) \delta_{pq}^{Kr} = \mathbf{V}_p$$

Lagrangian dynamics of a fluid parcel ($\delta M_p = 0$)

Eulerian discretized momentum eq.

$$\mathbf{g}_i^{n+1} - \mathbf{g}_i^n = -\nabla \cdot [\overline{\mathbf{g}\mathbf{u}} + \overline{[\nabla \cdot \mathcal{P}]_i}] \Delta t$$

Lagrangian: interpolate at p site: $(\sum_i \delta_{ip}^I \square)$

$$\Delta \mathbf{g}_p = \mathbf{g}_p^{n+1} - \mathbf{g}_p^n = \left(\mathbf{g}_{p^{n+1}}^n - \mathbf{g}_{p^n}^n \right) - \nabla \cdot [\overline{\mathbf{g}\mathbf{u}}_p + \overline{[\nabla \cdot \mathcal{P}]_p}] \Delta t$$

where $\delta \mathbf{g}_p \equiv (\mathbf{g}_{p^{n+1}}^n - \mathbf{g}_{p^n}^n) = \Delta \mathbf{R}_p \cdot \nabla_{\mathbf{R}} \mathbf{g}_{p^n} = \Delta t \overline{\mathbf{V}}_p \cdot \nabla_{\mathbf{R}} \mathbf{g}_{p^n}$

Explicit scheme (Euler):

$$\rho_p^{n+1} \frac{\Delta \mathbf{u}_p}{\Delta t} + \nabla \cdot \mathcal{P}_p^{n+1} =$$

$$\delta \mathbf{u}_p \nabla \cdot \mathbf{g}_{p^{n+1}} + \rho_{p^{n+1}}^n \left(\mathbf{V}_p^n - \mathbf{u}_{p^{n+1}}^n \right) \cdot \nabla \mathbf{u}_{p^{n+1}}^n = O(\rho u^3 \Delta t / l^2)$$

Semi-implicit (Crank-Nicholson):

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Eulerian-Lagrangian momentum consistency

Accuracy: differences in total fluid momentum gain in Eulerian and Lagrangian variables

- Eulerian momentum $\Delta \mathbf{W}_E = h^3 \sum_i \left(\Delta \mathbf{g}_i + \overline{\nabla \cdot \Pi}_i \Delta t \right)$

$$\Delta \mathbf{W}_E = \sum_i \sum_p h^3 \overline{\mathbf{F}_{ip}} \Delta t = \sum_p \overline{\mathbf{F}_p} \Delta t \quad (32)$$

Fluid+particle (*Eulerian*) momentum exactly conserved

- Lagrangian momentum

$$\Delta \mathbf{W}_L = \sum_p \overline{\mathbf{F}_p} \Delta t + O(\rho u^3 \Delta t^2 / h^2) \text{ (explicit scheme)} \quad (33)$$

Explicit scheme: limited to $Re < 1/CFD$ (Courant no.)

Semi-implicit: Lagrangian momentum error $O(\Delta t^3)$

Higher order schemes (open problem).

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Compressible fluid at low Mach number

- Trivial generalization of the spread force density

$$\overline{\mathbf{f}}_{ip} \Delta t = \rho_i [\mathbf{V}_p - \tilde{\mathbf{u}}_p] \delta_{ip}^S \quad (34)$$

- Particle-fluid force:

- **Eulerian**

$$\sum_i \overline{\mathbf{f}}_{ip} h^3 \Delta t = \rho_p \mathcal{V}_p [\mathbf{V}_p - \tilde{\mathbf{u}}_p] = \overline{\mathbf{F}}_p \Delta t \quad (35)$$

- **Lagrangian**

$$\sum_i \delta_{ip}^I \overline{\mathbf{f}}_{ip} h^3 \Delta t = \rho_p^* \mathcal{V}_p [\mathbf{V}_p - \tilde{\mathbf{u}}_p] = \overline{\mathbf{F}}_p^* \Delta t \quad (36)$$

with $\rho_p^* = \sum_i \rho_i \delta_{ip}^I \delta_{ip}^S$. recall that $\sum_i \delta_{ip}^I \delta_{ip}^S = 1$ so $\rho_p^* \simeq \rho_p$

Force inconsistency: $\delta F = |F - F^*|/F < 0.17\text{Ma}^2$.

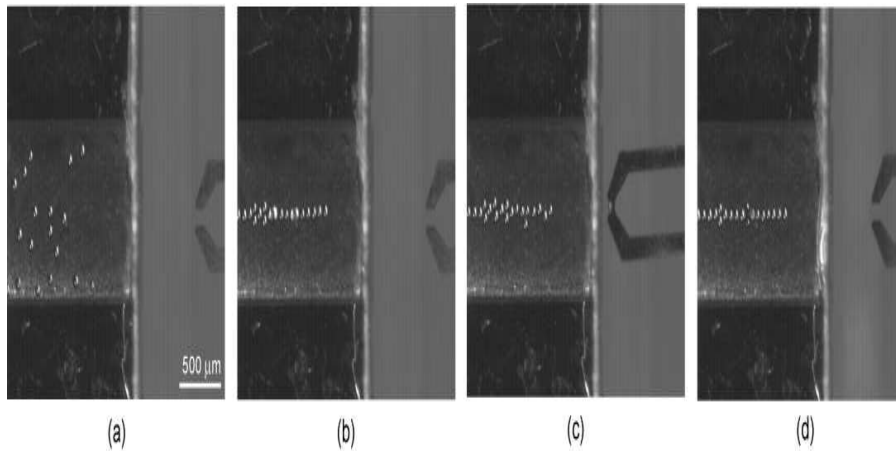
Scheme valid at low Mach number

Tests

- **Hydrodynamic radius:** $R_H = 0.9 h$ (translational invariance: $\text{Std}[R_h] \simeq 1\%$)
- **Drag force:** valid up to $\text{Re} \sim 10$ (equivalent to slippery surfaces)
- **Velocity profiles**
- **Hydrodynamic forces: Oseen and Lubrication**
- **Fluctuations**
- **Velocity autocorrelation:** long time tails
- **Acoustic force**

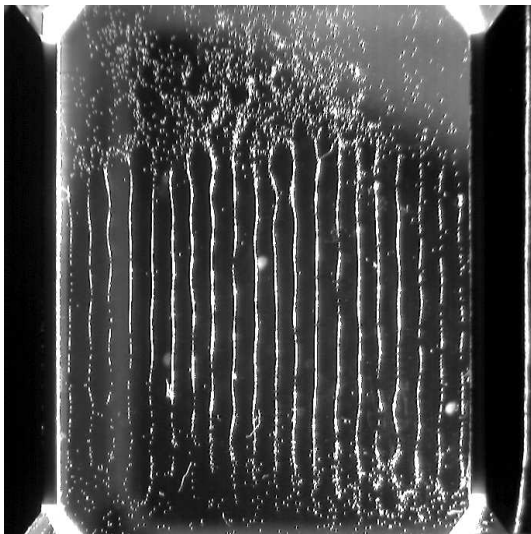
Sound-particle interaction

Micromanipulation of micron size particles with ultrasound. Jürg Dual group, ETH



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Sound-particle interaction

- A stationary sound wave generates an average force on a particle given by the gradient of a mean potential field $\langle \mathbf{F} \rangle = -\nabla \langle U \rangle$,

$$\langle U \rangle = 2\pi R^3 \rho_f \left(\frac{\langle \delta p^2 \rangle}{3\rho_f^2 c_f^2} f_1 - \frac{1}{2} \langle \delta u^2 \rangle f_2 \right) \quad (37)$$

- $f_1 = 1 - \rho_f c_f / (\rho_p c_p)$ and $f_2 = 2(\rho_p - \rho_f) / (2\rho_p + \rho_f)$
- Acoustic force for standing plane wave (wavenumber k , amplitude $\Delta\rho$)

$$\langle \mathbf{F} \rangle = \frac{\pi c_f^2 \Delta\rho^2 R^3 k}{\rho_f} \left(\frac{1}{3} f_1 + \frac{1}{2} f_2 \right) \sin(2kz) \hat{\mathbf{z}} \quad (38)$$

- Fit f_1 , f_2 and R from simulations: $c_p = c_f$ and $R = 1.19R_H$

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$$\langle U \rangle = 2\pi R^3 \rho_f \left(\frac{\langle \delta p^2 \rangle}{3\rho_f^2 c_f^2} f_1 - \frac{1}{2} \langle \delta u^2 \rangle f_2 \right) \quad (37)$$

- $f_1 = 1 - \rho_f c_f / (\rho_p c_p)$ and $f_2 = 2(\rho_p - \rho_f) / (2\rho_p + \rho_f)$
- Acoustic force for standing plane wave (wavenumber k , amplitude $\Delta\rho$)

$$\langle \mathbf{F} \rangle = \frac{\pi c_f^2 \Delta\rho^2 R^3 k}{\rho_f} \left(\frac{1}{3} f_1 + \frac{1}{2} f_2 \right) \sin(2kz) \hat{\mathbf{z}} \quad (38)$$

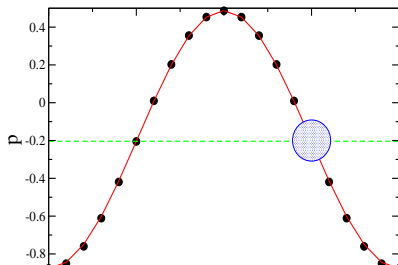
- Fit f_1 , f_2 and R from simulations: $c_p = c_f$ and $R = 1.19R_H$

Sound-particle interaction

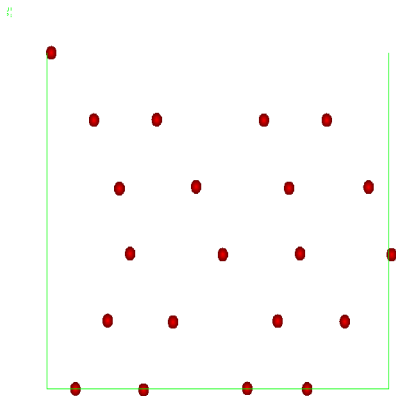
- Acoustic boundary layer $\delta = \sqrt{(\nu/\omega)}$, with $\nu = \eta/\rho$
- Wave number: $\lambda = c 2\pi/\omega$
- Particle radius: R_{NS}

Simulation

- $R_{NS}/\lambda \simeq 0.06$.
- Viscous effects: $\delta/R_{NS} \simeq 0.2$
- Stokes limit $\delta/R_H \gg 1$ is **not** valid. (Stokes coupling not suited)



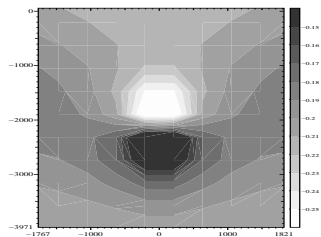
Sound-particle interaction



Animation

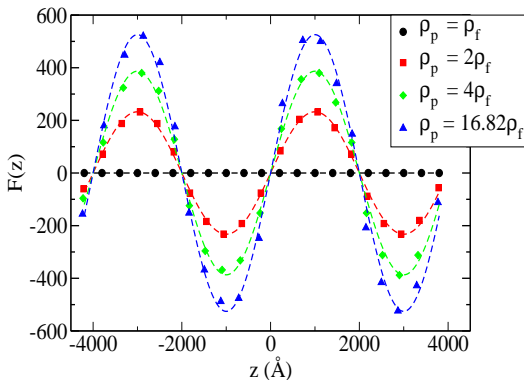
Direct forcing: pressure perturbation around particle

Mon Oct 18 23:42:08 2010



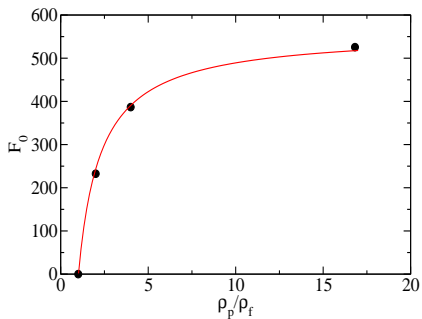
Acoustic force

Force of a standing wave at different positions



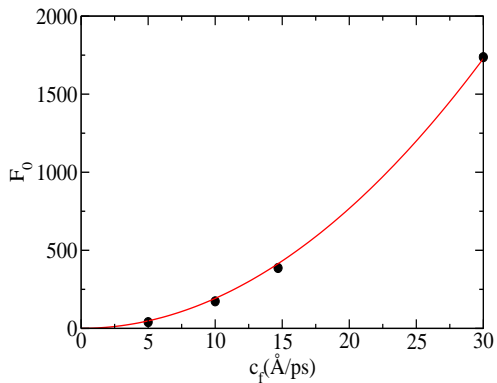
Acoustic force

Maximum force versus density ratio



Acoustic force

Maximum force versus fluid sound velocity



Stokes approximation for point particles

Review: Dünweg and Ladd Adv. Polym. Sci, 2008

Particle moving in an otherwise quiescent fluid, $\mathbf{u}_\infty = 0$

- Fluid-Particle force

$$\mathbf{F} = \xi_{bare}(\mathbf{V}_p - \mathbf{u}_p)$$

- Fluid velocity: $\mathbf{u}_p = T^{av}\mathbf{F}$

- Effective friction: $\mathbf{F} = \xi_{ef}\mathbf{V}_p$

$$\frac{1}{\xi_{ef}} = \frac{1}{\xi_{bare}} + \frac{1}{\xi_{hydro}}$$

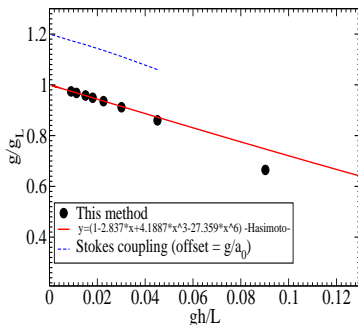
- Effective hydrodynamic radius: $R_H = 6\pi\eta/\xi_{ef}$

$$\frac{1}{R_H} = \frac{1}{a_0} + \frac{1}{gh}$$

with $a_0 = \xi_{bare}/(6\pi\eta)$ and $gh = \xi_{hydro}/(6\pi/\eta)$.

Finite size effects on $R_H = gh$

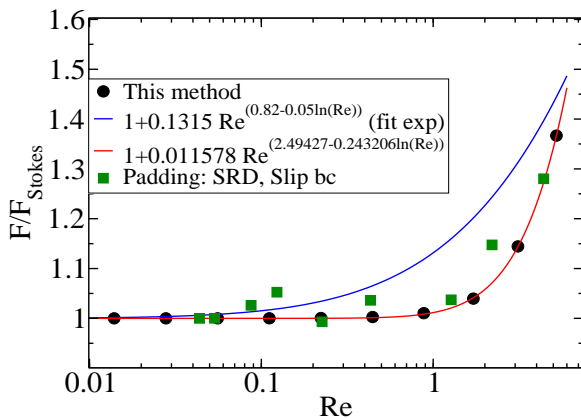
- Direct Forcing: $\frac{g}{gL} = 1 - 2.84 \frac{gh}{L} + \dots$
- Stokes coupling: $\frac{g}{gL} = \frac{6\pi\eta gh}{\xi_{bare}} + 1 - 2.84 \frac{gh}{L} + \dots$



Direct Forcing: strong coupling limit, instantaneous relaxation

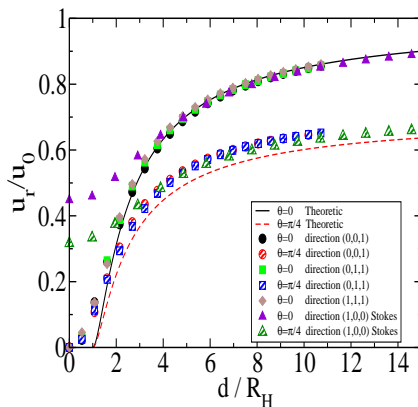
$$1/\xi_{bare} = 0$$

Drag at finite Reynolds number



Velocity profile around particle: PBC

Deviations at large distances are due to finite size effects.

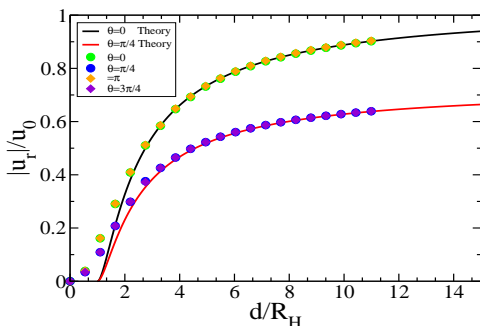


(Lines: analytic solution for $Re = 0$)

Velocity profile around particle: fixed velocity BC

To check for finite size effects we fix the fluid velocity \mathbf{u}_0 at the core of a spheric shell around the particle of radius r_s

$$\mathbf{u}(|\mathbf{r} - \mathbf{R}_p| = r_s) = \mathbf{u}_0$$



(Lines: analytic solution for $Re = 0$)

Forces between two particles: Oseen and Lubrication forces

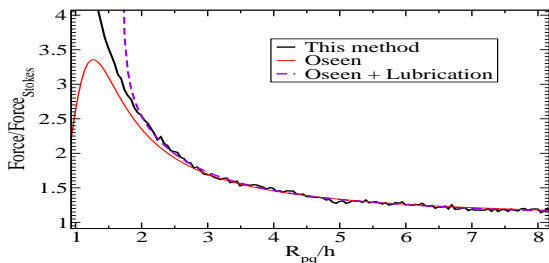
Particles with same hydrodynamic radius

Oseen force: $R_H = 0.9h$

Lubrication: best fit with $R_L = 0.92R_H$

$$F^l = -6\pi\eta \frac{R_1^2 R_2^2}{(R_1 + R_2)^2} \left(\frac{1}{s} - \frac{1}{s_c} \right) (\mathbf{V}_1 - \mathbf{V}_2) \hat{\mathbf{R}}_{12} \hat{\mathbf{R}}_{12} \text{ for } s < s_c$$

with $s = |R_{12}| - R_1 - R_2$

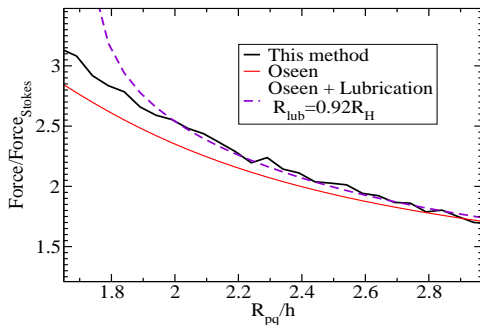


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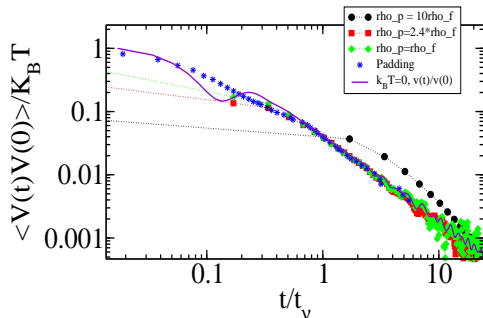
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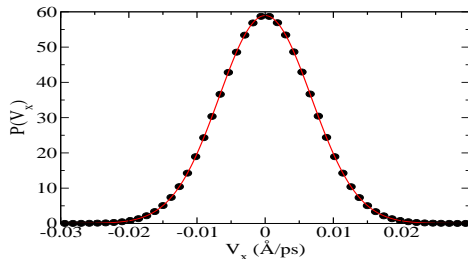


Direct forcing: Velocity decay and long-time tail



Particle within Fluctuating Hydrodynamics

- Particle kinetic temperature thermalizes with fluid
- There is no dissipative channel in the particle motion, as happens in Stokes coupling
- **No need** for Langevin force in the particle motion



Conclusions

Direct forcing for pointwise particles

- Fluid-Particle force from imposition of no-slip at particle site.
 - Generalization of Stokes coupling method (strong coupling limit)
 - Processes involving fast momentum transfer friction time
-
- Particle inertia is taken into account
 - Wall b.c. of arbitrary shape (first order accuracy). Easily generalized to elastic boundaries (IB with inertia)
 - *Fluctuating hydrodynamics*: Fluid momentum fluctuations are transmitted to the particles without dissipation: "particle thermostat" is not required.

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Implementation

- No-slip implemented in **one-step** (no iterations).
- **The algorithm**: easy to implement from a Stokes code
- Parallelizable and written in CUDA (GPU): (50-100 faster than in a single CPU)

Formalization (in colab. Aleks Donev)

- Projection operators
- Fluctuation-dissipation balance

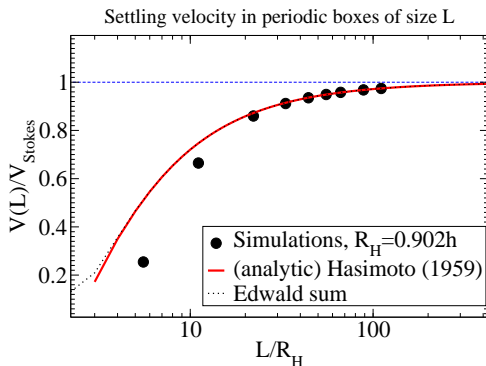
Applications (too many)

- Manipulation of colloids using ultrasound
- Particle dispersion in turbulent flow: memory effects, finite particles
- Effects of hydrodynamics on colloidal fluid gelation (E. Del Gado, ETH)

Calculation of g : finite size effects

- Settling velocity of a periodic array of particles with interparticle distance L (Hasimoto, 1959)

$$\frac{V_L}{V_\infty} = 1 - 2.84 \frac{R_H}{L} + 4.1887 \frac{R_H^3}{L} - 27.359 * \frac{R_H^6}{L} + ..$$



Calculation of g : finite size effects

- If the Stokes relation is assumed in PBC, $R_H = gh$ has to be redefined, $R_H^L \equiv g_L h$, with

$$\frac{g}{g_L} = \frac{V_L}{V_\infty} = 1 - 2.84 \frac{gh}{L} + \dots$$

Hydrodynamic Radius in Direct forcing

- Simulations:
 - PBC box of size L .
 - Particle: constant external force $\mathbf{F}_{ext} = F_{ext}\mathbf{k}$
 - Fluid: external pressure gradient $\partial p_{ext}/\partial z = F_{ext}/L^3$
 - Total momentum conserved
 - Steady state $F_{ext} = F_{drag}$, $\mathbf{V}_p = \mathbf{V}_p^{lim}$ and $\mathbf{u}_\infty = \mathbf{u}_\infty^{lim}$.
 - The hydrodynamic radius R_H is defined via the Stokes drag

$$\mathbf{F}_{drag} = 6\pi\eta R_H(\mathbf{V}_p - \mathbf{u}_\infty)$$

- Results
 - $R_H = gh$
 - $g = (0.89 \pm 0.05)$

Translational invariance: g

Quite small variation of g in mesh: $Std[g] \leq 0.01\bar{g}$

